

COMBINATION FILTRATION FOR REMOVING DIVALENT SALTS AND CONTAMINANTS FROM MONOETHYLENE GLYCOL (MEG) RECLAMATION UNITS

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- Amine Filtration for SO₂ Scrubbing
- Amine Filtration for CO₂ Scrubbing
- Water Scrubbing-Downstream of Clarifiers
- Grey Water Filtration
- Gasification
- Bioenergy / Biochemical
- MEG Filtration

BHS Concentrating Candle Filters & Pressure Plate Filter: Amine Filtration





BHS Candle Filters with Activated Carbon for Amine Filtration







BHS Candle Filters for Amine Sweetening

TRANSFORMING MATERIALS INTO VALUE







Downstream of Clarifiers for Water Scrubbing



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Downstream of Clarifiers for Water Scrubbing



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BHS Candle Filters-Amine Sweetening from Coker & Cracker Streams





BHS Concentrating Candle Filters for Grey Water from Coal Gasification



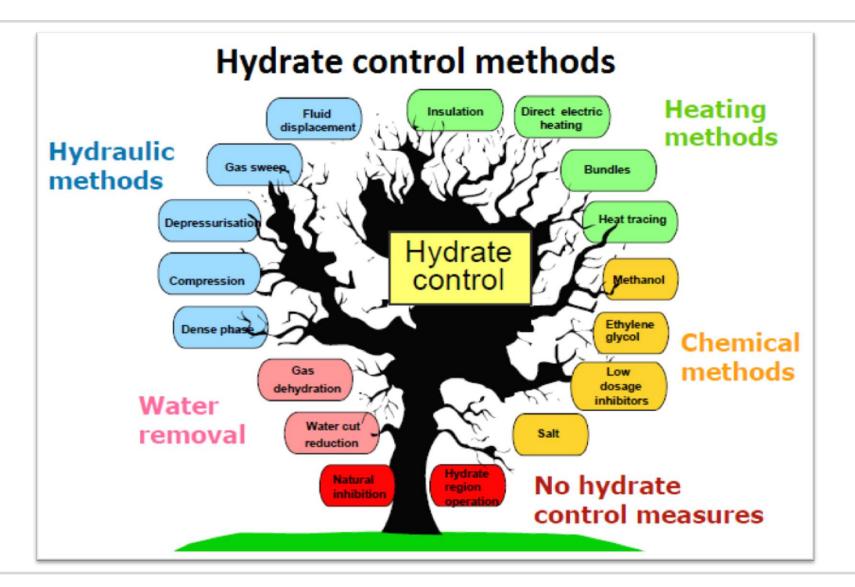




- In the natural gas industry hydrate formation is a well known problem which requires close attention and follow-up.
- It may cause slower gas flow and finally block the gas pipe flow and stop the production.
- It may also damage equipment and create safety issues and extra cost.

Presentation Overview





Introduction



- MEG (Mono Ethylene Glycol) is used as a hydrate and corrosion inhibitor in natural gas pipelines.
- After separation of the gas, "rich MEG" (MEG and formation water) is treated in reclamation units to recover the MEG.
- The rich MEG is regenerated into a lean, high purity, salt-free MEG for reuse
- Carbonates and Hydroxides from mono and divalent cations precipitate during evaporation of the water.
- The precipitated salts lead to clogging in pipes and heat exchangers.



Typical Process Parameters for MEG Reclamation



- Suspended Solids Content in Rich MEG: 50-1000 ppm (divalent salts, corrosion products, debris and other solids)
- Particle size distribution: 5-50 µm
- Temperature: 50 80 °C

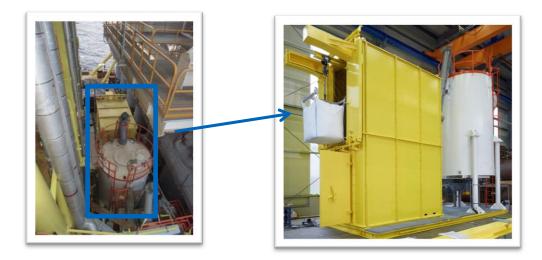
SELECTION OF FILTRATION TECHNOLOGY FOR MEG PROCESS



- Filtration of the Rich MEG for Regeneration
 Filtration of the Salt Brine
 - Candle Filtration with Precoat for Varying Process Conditions & Hydrocarbons
 - Combination of Alternative Concentrating Technologies (static thickeners, disc stack centrifuges, decanter centrifuges) followed by Pressure Plate Filtration
 - New BHS Option: Combination of Concentrating Candle Filtration and Pressure Plate Filtration

BHS Candles Filters with Precoat: Offshore in South China Sea

Three Candle Filters
Mono Ethylene Glycol
Filtration for Regeneration

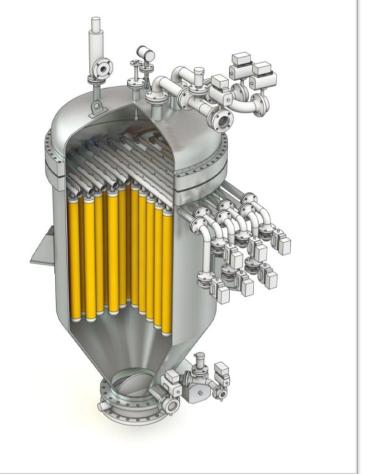




Conventional Single-Stage Process: Precoat Filtration with Candle Filters

- Candle filters: Displace MEG from the solids by drying with compressed gas (typically N_2).
- Due to the low solid content a precoat layer (Perlite) is applied before filtration.
- The separated salts and precoat can be discharged as a dry filtercake.









 Combination of Alternative Concentrating Technologies (static thickeners, disc stack centrifuges, decanter centrifuges) followed by Pressure Plate Filtration

- Pressure Plate Filters: Maximum efficiency for cake wash due to the horizontal filter plates.
- MEG is displaced by water.
- The separated and washed salts can be discharged as a dry filtercake.
- A further significant reduction of MEG in the filter cake is possible.







- Combination of Alternative Concentrating Technologies (static thickeners, disc stack centrifuges, decanter centrifuges) followed by Pressure Plate Filtration
- Problem: High-speed separators and centrifuges have high wear due to the abrasive salts; high costs and energy usage; & dynamic loads.

BHS Objective is to Improve the Filtration, Washing & Drying



- Solving a filtration problem for divalent salts based upon BHS amine experience:
 - Lab testing, Pilot testing & Scale-Up,
 - Performance Guarantees
- Lab Testing Results
 - Cake Thickness and Filtration
 - Filter Media
 - Cake Washing
 - Cake Drying
 - Cake Discharge

BHS Laboratory Tests







SELECTION OF FILTRATION TECHNOLOGY FOR MEG PROCESS

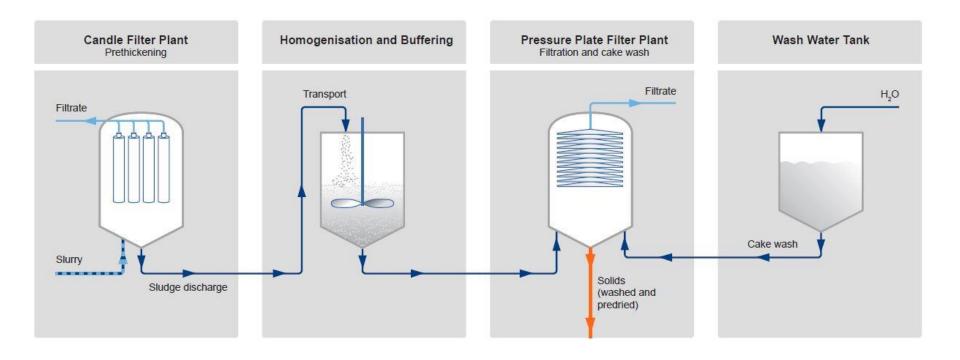


BHS Process Development: Combination Process Based Upon Amine Filtration Experience

- Concentrating Candle Filtration
 Followed By
- Pressure Plate Filtration for
 - Final Washing for MEG removal
 - Final Drying for Salt Disposal
 - No Free Liquid



The Process Operation





Concentrating Candle Filters (60 m²)to Pressure Plate Filtration (8 m²)-Typical Reduction

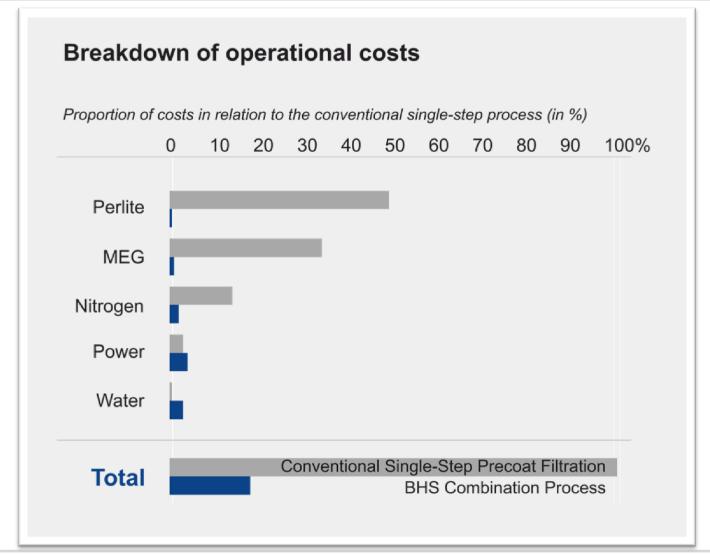




Comparison of Capital and Operating Costs

- Investment costs are about 30% less than the Conventional Single Stage Process with Precoat
- Operating Costs are about 80% less
 - No filter aid (no Perlite consumption)
 - Lower MEG replacement
 - Low energy usage (Low Nitrogen consumption)
 - Low wash water usage
- Finally, the Combination Process
 - Reduces MEG loss by a factor of 30 (High MEG Recovery)
 - Provides dry salt for discharge





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